

# New Approaches to Reacting Flow Modeling for Endothermic Fuel Cracking and Combustion in High-Speed Combustion

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# Objectives

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## Intermediate term

Mechanisms of early-stage homogeneous coking and methods to suppress PAH coalescence/reaction.

## Long term

Enable new approaches to kinetic modeling.

# The Problem

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JP7

## Endothermic cooling system

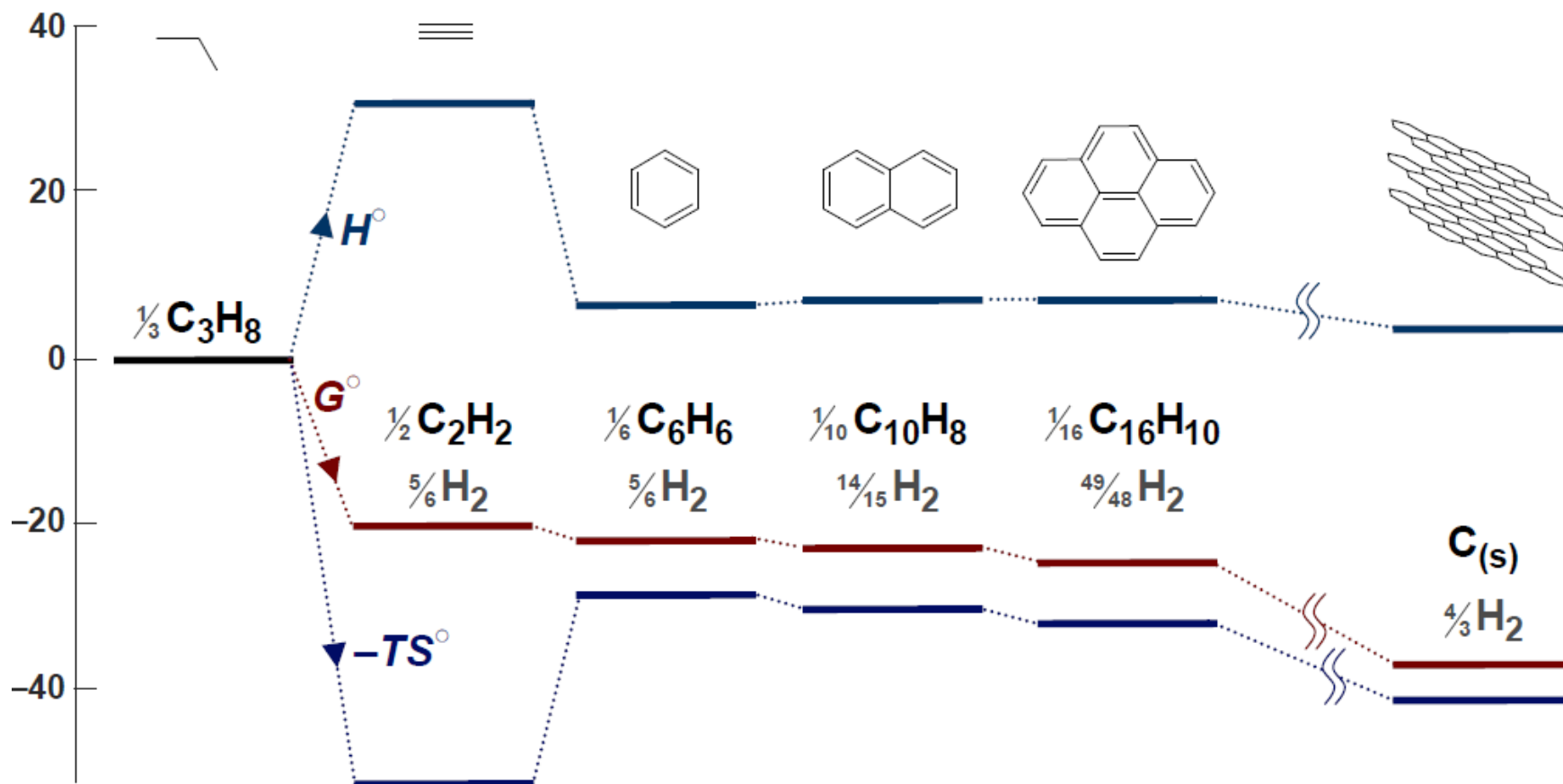
- Fuel pyrolysis to remove heat
- Cracked products give better combustion performance
- Coke formation is a problem
- May use catalysts

## Combustor

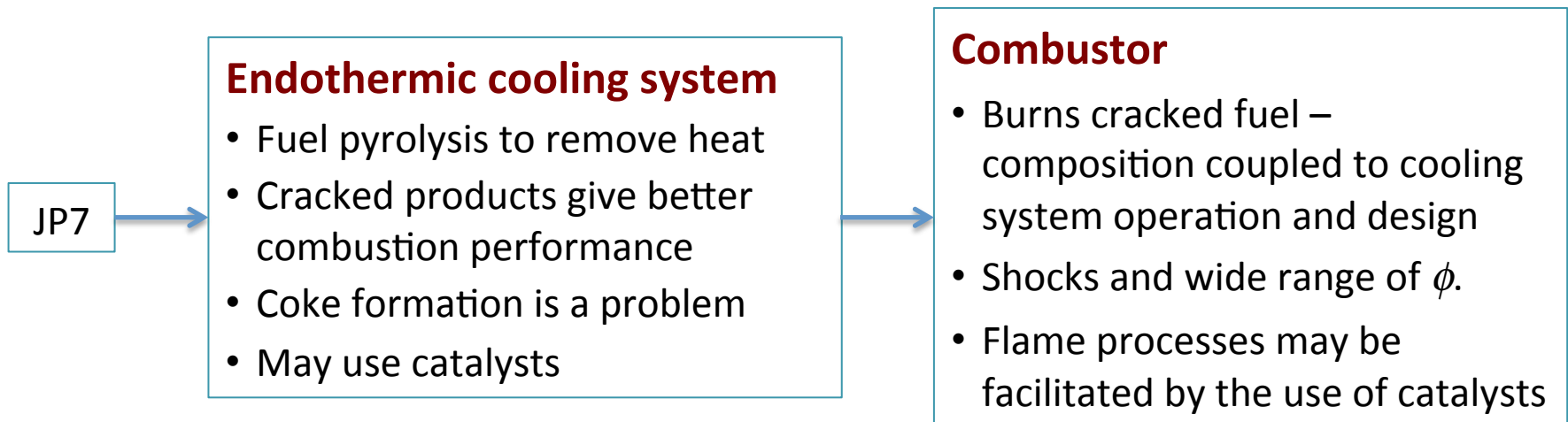
- Burns cracked fuel – composition coupled to cooling system operation and design
- Shocks and wide range of  $\phi$ .
- Flame processes may be facilitated by the use of catalysts

- Fuel cracking in the cooling system gives heat sinking capability, but also promote coke formation.
  - Fuel cracking and coke formation driven by the same force – entropy!

# Thermodynamic Driving Forces

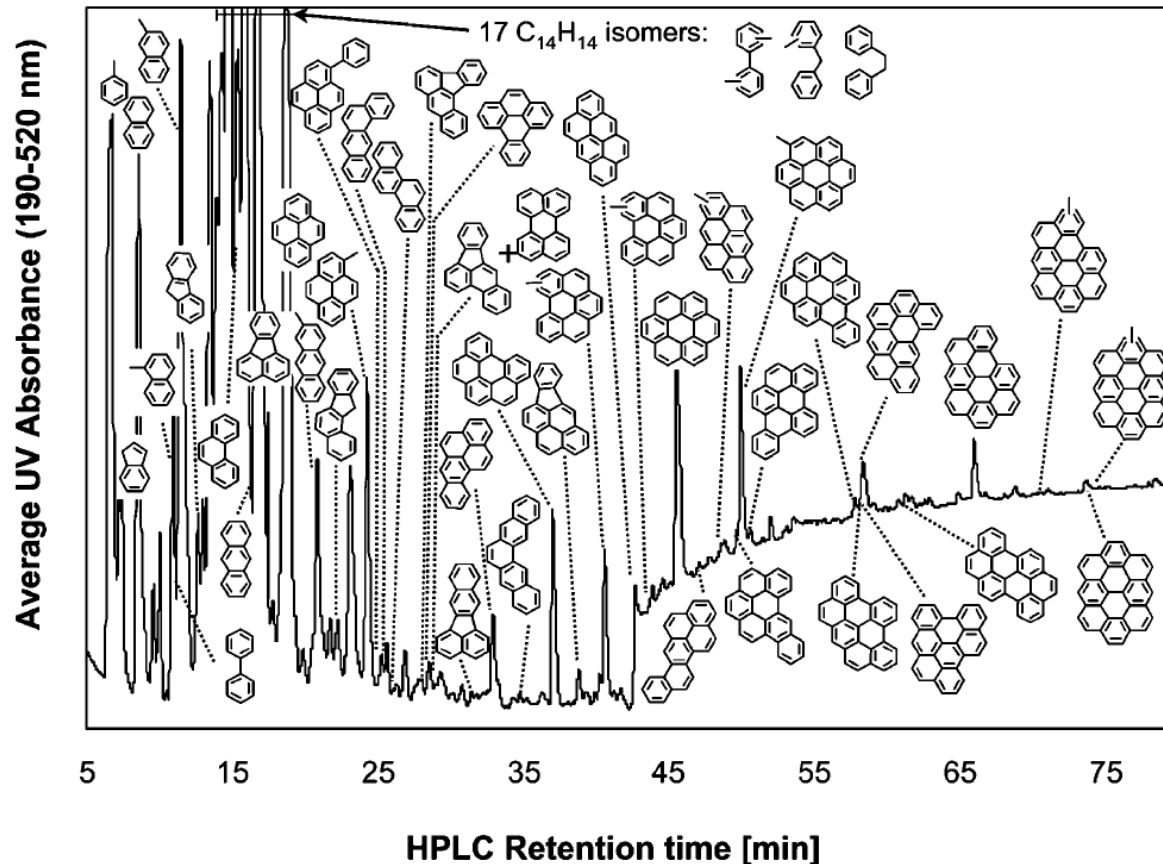


# The Problem



- Fuel cracking in cooling system gives heat sinking capability, but also promote coke formation.
  - Fuel cracking and coke formation driven by the same force – entropy!
  - The processes are kinetically controlled (and supercritical).
- Three types of coke deposits (**Edwards 2003**)
  - **Filamentous** – fluid/surface interactions in origin and controllable by surface materials engineering).
  - **Amorphous and graphitic** – PAHs formed in the fluid phase “coalesce” into particulates which deposit on walls – a key problem to be addressed.

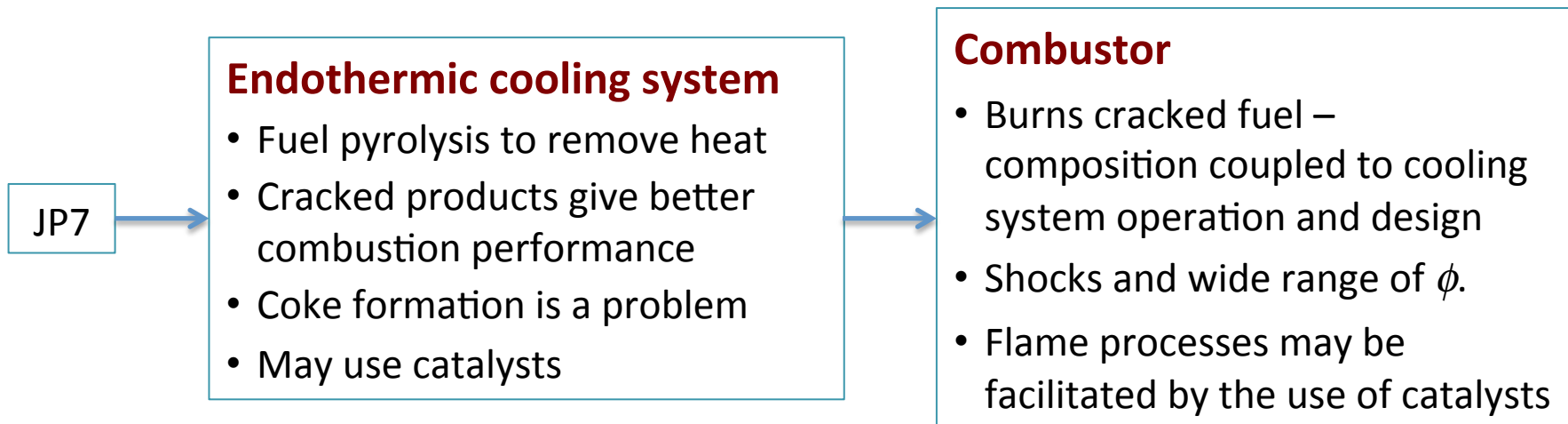
# PAHs as Intermediates to Coke



Wornat (2007)

- Amorphous and graphitic wall deposits are presumably from particulate matters due to PAH-PAH coalescence/reaction.
- PAH binding mechanisms not well established: dispersion/electrostatic interactions, excited states, dynamic bonding etc.

# The Problem



- Fuel cracking in the endothermic cooling system gives better heat sinking capability, but also promote coke formation.
  - Fuel cracking and coke formation driven by the same force – entropy!
  - The processes are kinetically controlled.
- Three types of coke deposits
  - **Filamentous** – fluid/surface interactions in origin and controllable by surface materials engineering).
  - **Amorphous and graphitic** – PAHs formed in the fluid phase “coalesce” into particulates which deposit on walls – a key problem to be addressed.
- A highly coupled kinetic problem – how do we generate chemical reaction models directly from results of *ab initio* theory?

# Working Hypotheses/Questions(1)

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## The Coking Problem

1. Fuel pyrolysis and PAH/coke formation share the same thermodynamic driving force. It is impossible to maximize fuel pyrolysis while suppress PAH formation at the same time.
2. Suppressing PAH-PAH coalescence/reaction is feasible, because such processes do not yield large Gibbs free energy drop.
  - Fundamental binding interactions among PAHs (purely dispersion/ electrostatic forces or also involves other *unknown* interactions – electronically excited states,  $\pi$  diradicals etc).
  - Dynamic effects under supercritical condition.
  - If these interactions/effects can be understood, is there an additive that can trick PAHs into disliking each other.



## Working Hypotheses/Questions(2)

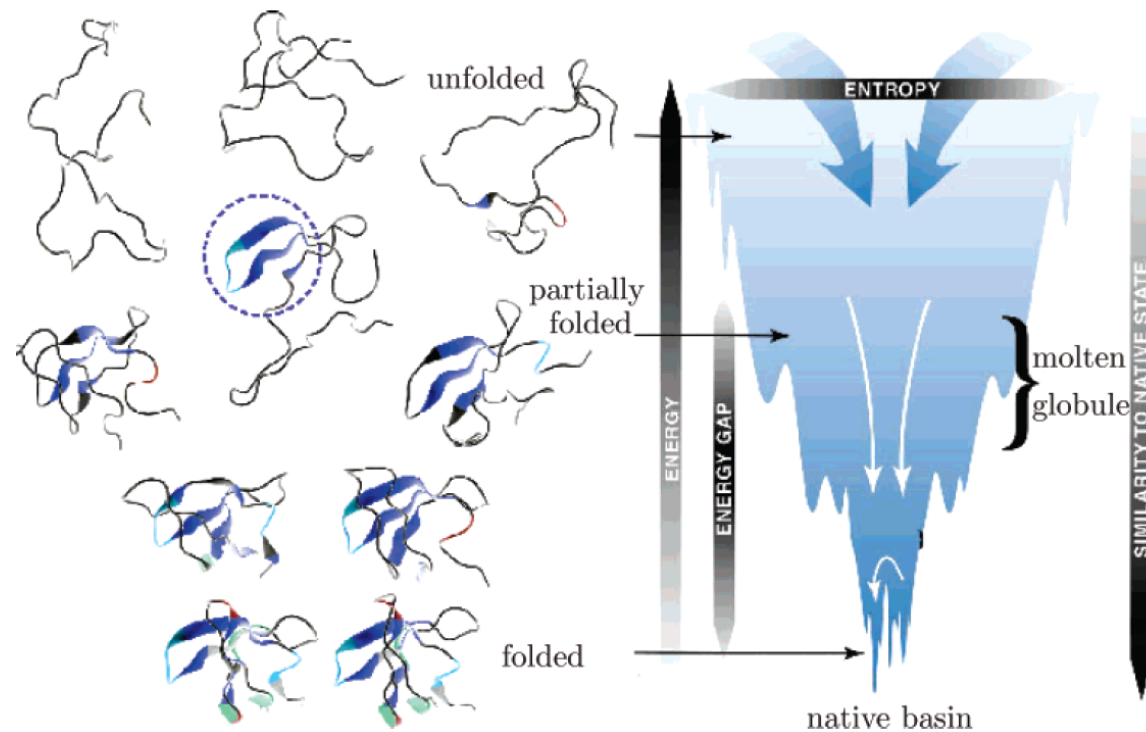
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### The Long-Term Combustion Chemistry Problem

1. Looking for an approach more robust and more “*ab initio*” than the current chemistry modeling approach.
  - Designs of endothermic cooling system and combustors are evolving;
  - New catalysts are being developed
  - Long lead-time to develop any predictive, coupled kinetic models
  - High pressure/supercritical kinetics – rate theory (and its application) falls apart.
  - .....
2. We have been using the approach of detailed kinetic modeling for more than 50 years.
  - Is this the only “fundamental” approach we can take?
  - Do we need to write out thousands of reactions before we can make a prediction about the kinetic and heat release rates?

# Potential Energy Landscape and Associated Approaches

- A concept widely used in protein folding kinetics (Joseph Bryngelson)

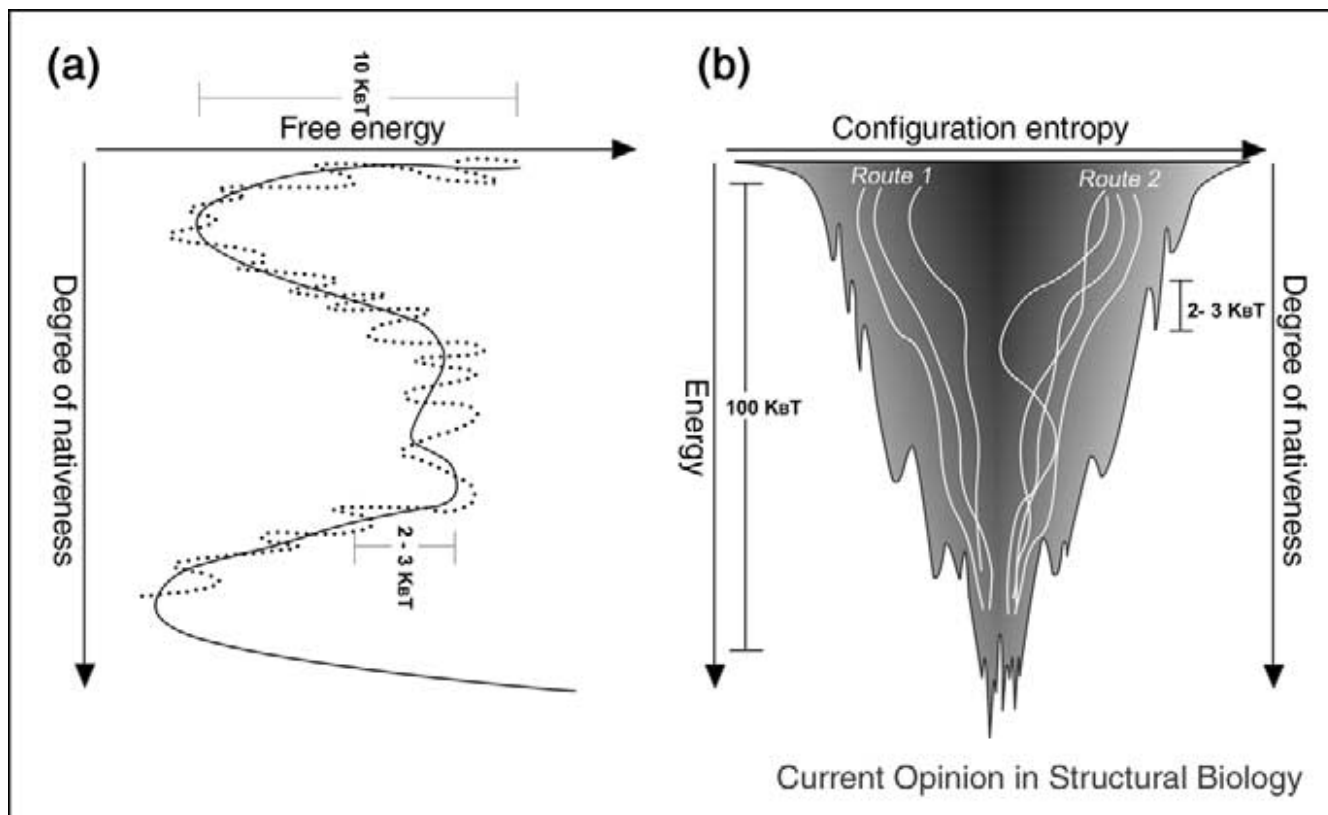


Wales & Bogdan *JPCB* (2006)

- and in materials/fuel cell research.

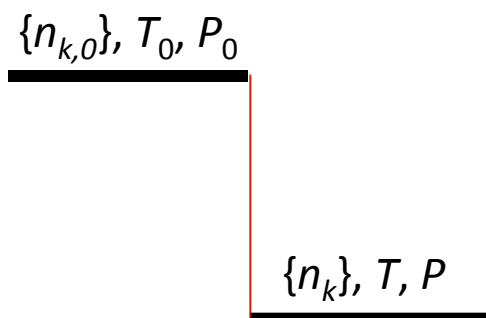
# Potential Energy Landscape and Associated Approaches

- Accuracy of kinetic prediction may be improved, as needed, by adapting the resolution of potential energy.



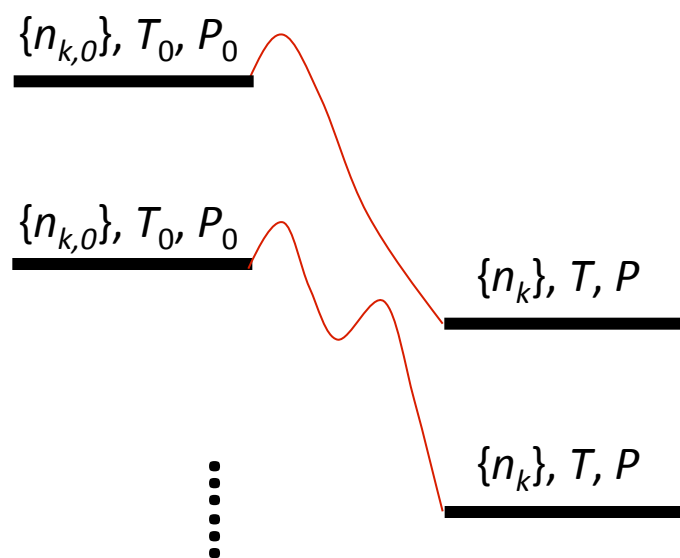
Onuchic & Wolynes *Current Opinion in Structural Biology* (2004)

# RCCE and Potential Energy Landscaping (RCCE-PEL)



## ***0<sup>th</sup> order potential energy landscape***

- No reaction steps  $\rightarrow$  Infinite rate kinetics
- The end state represents chemical equilibrium



## ***Higher-order potential energy landscapes***

- Slow(er) reaction steps added – equivalent to adding details (barriers and local minima) into the potential energy landscape
- Finite rate kinetics with accuracy improved by an adaptive approach to adding PES details
- Converging chemical time scale  $\leftrightarrow$  physical time scale (flow, turbulence, transport)

# The Team

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**Guillaume Blanquart**  
CalTech

- PEL-RCCE in turbulent reacting flow modeling



**Ronald K. Hanson**  
Stanford

- Experimental method developments  
 $T(t)$ ,  $H(t)$ ,  $S(t)$ ,  $G(t)$



**William L. Hase**  
Texas Tech

- Chemical dynamics  
aromatic interactions and binding  
post-transition state dynamics



**Keiji Morokuma**  
Emory/Kyoto U.

- Automated PES search methods



**Hai Wang**  
USC

- PEL-RCCE theory and application
- PAH-PAH binding interactions/coalescence suppression
- Nanocatalysts

# Rate-Controlled Constrained-Equilibrium (RCCE)

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Keck & Gillespie (1971); Keck (1990); Beretta et al. (2012)

The method of Lagrange Multipliers as applied to chemical equilibrium

$$L = \frac{G}{R_u T} + \sum_{m=1}^M \lambda_m \left( \sum_{k=1}^K a_{mk} n_k - e_m \right)$$

The equilibrium composition is given as

$$\begin{aligned} n_k &= n_0 \exp \left[ -\frac{g_k^0(T)}{R_u T} - \ln \frac{p}{p^0} - \sum_{m=1}^M \lambda_m a_{mk} \right] \\ &= n_0 Q_k \exp \left[ -\sum_{m=1}^M \lambda_m a_{mk} \right] \end{aligned}$$

where the multipliers are solved by

$$\begin{aligned} e_m &= n_0 \sum_{k=1}^K a_{mk} Q_k \exp \left[ -\sum_{m=1}^M \lambda_m a_{mk} \right] \quad (m = 1, \dots, M \text{ elements}) \\ 1 &= \sum_{k=1}^K Q_k \exp \left[ -\sum_{m=1}^M \lambda_m a_{mk} \right] \end{aligned}$$

# Rate-Controlled Constrained-Equilibrium (RCCE)

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**Keck & Gillespie (1971); Keck (1990); Beretta et al. (2012)**

For non-equilibrium problems, additional constraints are added as needed, preferably starting from rate limiting steps:

$$e_l = \sum_{k=1}^K a_{lk} n_k \quad (l - m = 1, \dots, R)$$
$$\frac{d(e_l/V)}{dt} = \sum_{k=1}^K a_{lk} \frac{d(n_k/V)}{dt}$$
$$= \sum_{k=1}^K a_{lk} \left( \sum_{l=1}^{s_l} \nu_{kl} R_{lf} - \sum_{l=1}^{s_l} \nu'_{kl} R_{lb} \right)$$

- Yields the exact solution when the number of constraining equations  $R$  = number of reactions  $I$  (Keck 1990).
- Good quality, converging solution achieved usually with  $R \ll I$ .
- A mechanism reduction method – allowing for separation of time scales – still require a (detailed) reaction mechanism to be made available.

# Principle Questions Yet to be Addressed

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- Can a potential energy landscape (PEL) approach be developed from ab initio methods?
- Can the rate limiting steps on the PEL be identified in a robust manner?
- Can new experimental approaches be developed to interrogate parts of a PEL?
- What are the role of the better known  $\text{H}_2/\text{C}_1\text{-C}_4$  chemistry in the RCCE-PEL approach?
- Can the RCCE-PEL approach be implemented in turbulent flame simulations?



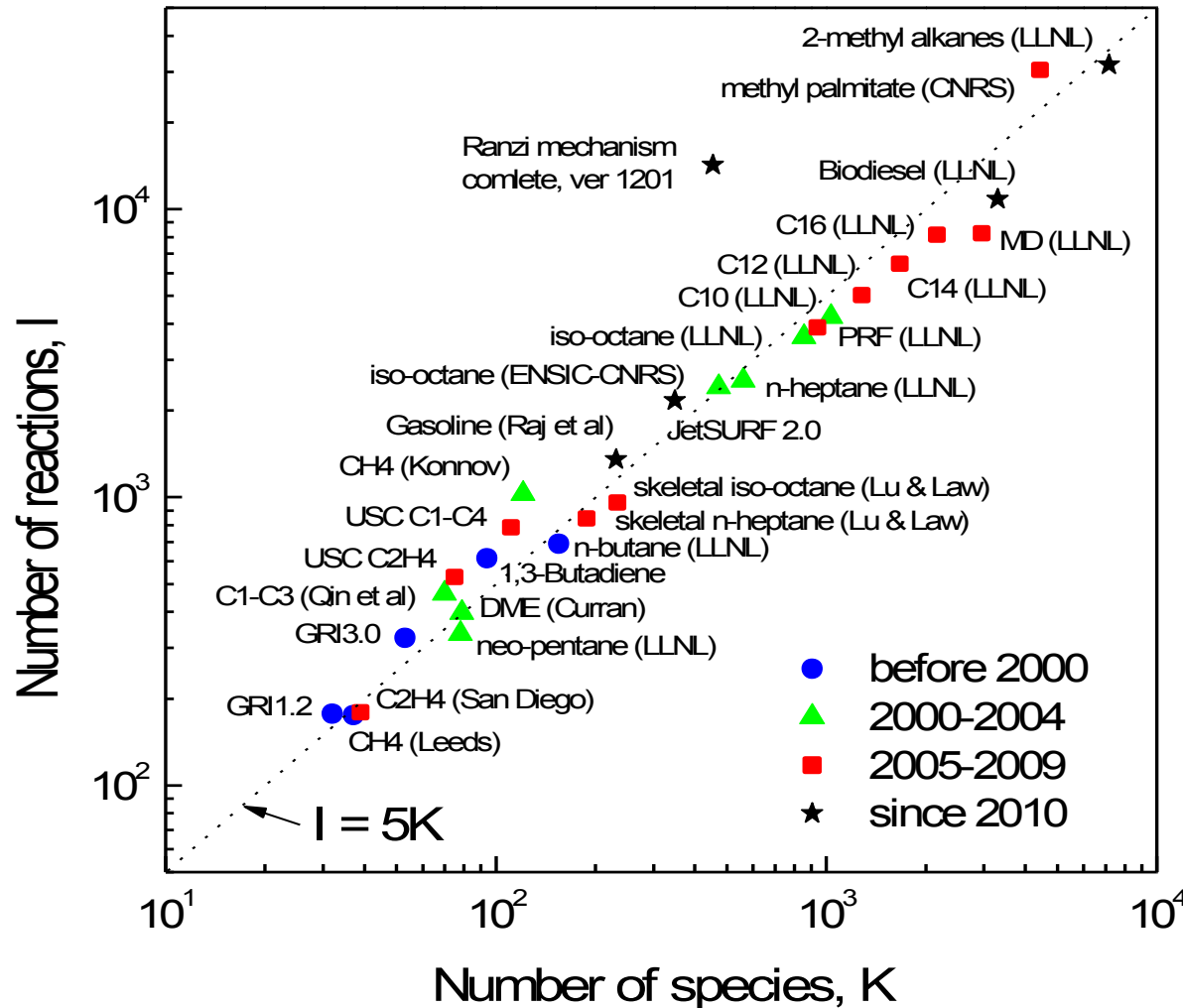
# Current Approach

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- Methodology based on Dixon-Lewis' s work in the 1960s' .
  - Write down every reaction step and find its rate coefficient.
  - $\text{H}_2$ ,  $\text{H}_2/\text{CO}$  etc with  $\sim 2$  dozen reactions.
  - Can have a closure because of a limited number of rate parameters.
  - Allowed us to understand the detailed laminar flame structure.
- Later work by many focused on combustion chemistry of small hydrocarbons –  $\text{O}(100)$  reactions – many of which have been probed directly by experiments and rate theory calculations.
- Recent effort for large hydrocarbons largely based on empirical knowledge
  - group additivity
  - analogous reactions – reaction class
  - guesses

# Current Approach

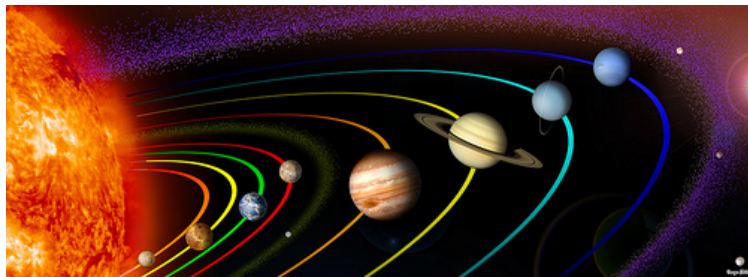
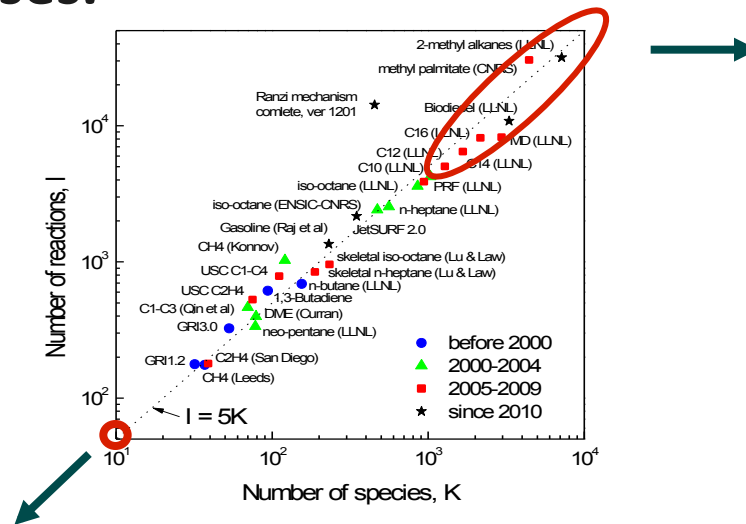
- The number of species/reactions increases exponentially as the fuel size increases.



An updated version of Lu & Law, 2009

# Current Approach

- The number of species/reactions increases exponentially as the fuel size increases.



- A solar system model built on the position and velocity of each and every planet is a triumph of science.
- A milky-way galaxy model built on the position and velocity of each planet and star is probably a terrible model.

# Combustion Reaction Mechanism Development

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- **Methods of mechanism reduction becomes mature.**
  - Still require detailed reaction models to be made available
  - The number of scalars remain large, perhaps too large to incorporate in CFD codes (high-speed combustion) for years to come
- **Rethink our strategy for treating chemistry.**
  - Adaptive resolution/accuracy
  - Key property to follow: time evolution of energy and entropy
- **Throw away the concept of reaction mechanism for the moment**
- **Focus on the potential energy surface**
  - some initial thoughts in the context of Keck's RCCE